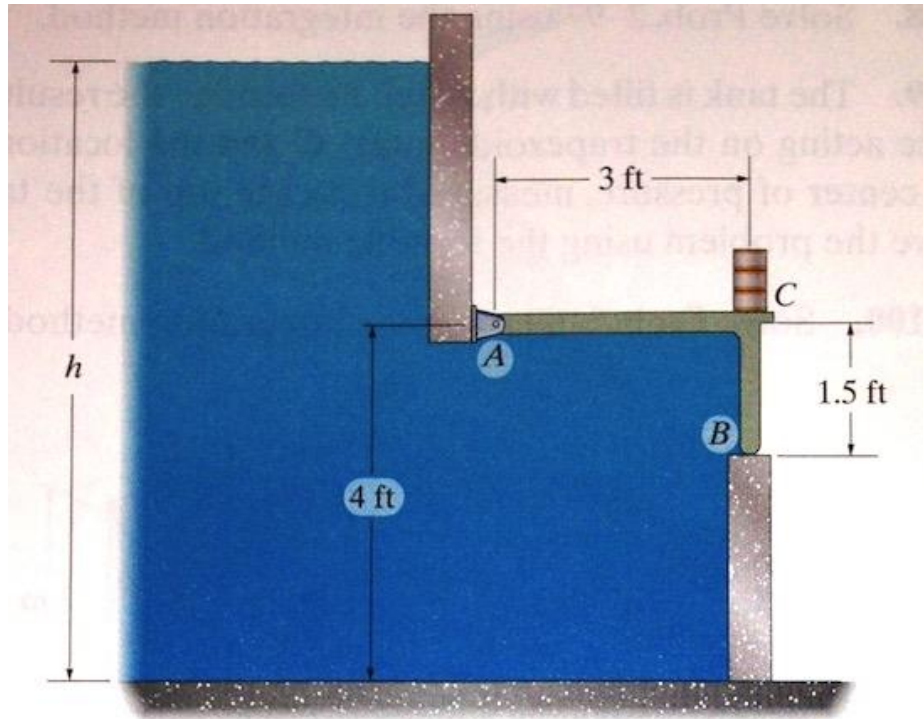


1. The control gate ACB is pinned at A and rests on the smooth surface B . If the counterweight C is 2000 lb, determine the maximum depth of water h in the reservoir before the gate begins to open. The gate has a width of 3 ft and has negligible mass compared to the counterweight.

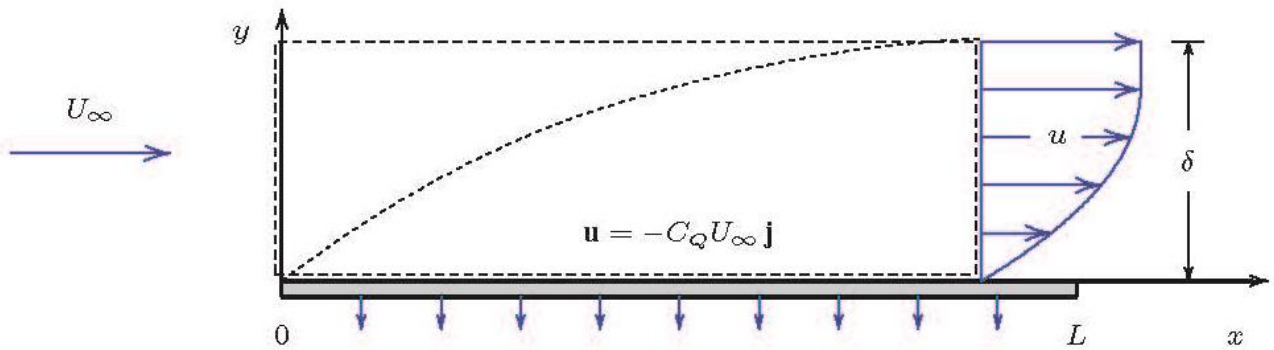


2. The aortic arch can be considered as a curved tube with pulsatile flow. Some dimensional variables are the diameter of the tube, D , the length of the tube L , the radius of curvature, r , the pulsatile frequency, f , the dynamic viscosity of blood, μ , the density of the blood, ρ , mean velocity in the tube, V , and the time of the experiment, T .

- a) Derive four independent non-dimensional parameters that would apply to this fluid dynamic situation. Choose the parameters for relevance to the dynamic behavior of the flow. Optional: Do you know the common names of these non-dimensional numbers?
- b) It is sometimes useful to model a flow situation in a laboratory with another fluid, such as water. Assuming we keep the dimensions of the model the same as the true aorta, if the kinematic viscosity of water is $\frac{1}{4}$ the kinematic viscosity of whole blood, what should be the mean velocity of water in the experiment to simulate the fluid dynamics?
- c) It is common for hemodynamicists to use an alternate form of a non-dimensional parameter called the Womersley number for pulsatile flows in tubes: $Wo = R \sqrt{2\pi f \rho / \mu}$, where R is the tube radius and $2\pi f$ is the angular frequency. Can you combine some of the parameters you chose in Part **a** to derive the Womersley number? What is the interpretation of force balance for the Womersley number?
- d) We would like to simulate the pulsatile nature of blood, but use water instead. What should the frequency of pulsatility be for the water model, using dimensional similarity?
- e) If we are to quantify **the shear stress** of the fluid on the aortic wall, is any conversion necessary from the laboratory measurements to the true aorta?

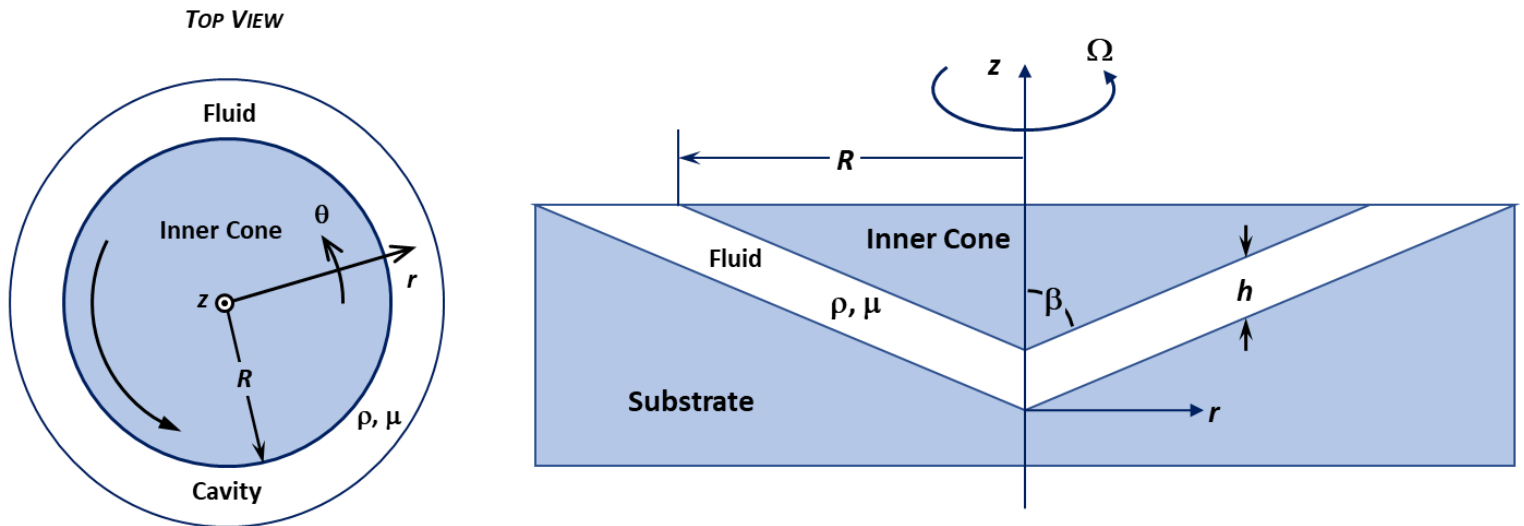
3. Consider steady, incompressible, viscous flow above a flat plate of length L with surface mass removal, which is referred to as suction. The velocity above the plate is given by $u(x, y) = U_\infty f\left(\frac{y}{\delta}\right)$ where U_∞ is the constant freestream velocity and $\delta(x)$ is the thickness of the viscous region. Pressure is constant and equal to p_∞ and you can assume that $u = U_\infty$ for $y \geq \delta$. The surface velocity is given by $\mathbf{u} = -C_Q U_\infty \mathbf{j}$, where C_Q is the constant suction coefficient. Show that, with ρ denoting fluid density and $\dot{m} = \rho U_\infty C_Q L$, the drag force per unit width out of the page is

$$F_D = \dot{m} U_\infty + \int_0^\delta \rho (U_\infty - u) u \, dy$$



You can use the stationary rectangular control volume shown in the figure for analysis.

4. A pointing down cone with the outer radius R is located a small distance above a conical cavity in the substrate. The cone and the cavity are concentric and have an equal half-angle of β . The cone rotates at a constant angular speed Ω . The gap between the cone and the cavity has a constant vertical (z) dimension of h , and is completely filled with a Newtonian fluid of constant density ρ and constant viscosity μ . Assume that the flow is steady, unidirectional, laminar, and $h \ll R$.



- What are the no-slip boundary conditions on the velocity field \vec{V} for the flow in the gap between the cone and the cavity?
- List all additional assumptions (beyond those given in the problem statement), and simplify the relevant governing equations. In words, what drives this flow?
- Determine the velocity field \vec{V} . Note that you are not required to solve the governing equations. Hint: use the boundary condition at the cavity surface to “guess” the form of the velocity field that ensures that this no-slip condition is automatically satisfied.
- Determine the shear stresses for this flow.
- What are \vec{V} and the shear stresses for this flow in the limit where $\beta \rightarrow \pi/2$?

For your reference, the Navier-Stokes equations in cylindrical polar coordinates are:

$$\rho \left(\frac{\partial V_r}{\partial t} + V_r \frac{\partial V_r}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_r}{\partial \theta} - \frac{V_\theta^2}{r} + V_z \frac{\partial V_r}{\partial z} \right) = -\frac{\partial p}{\partial r} + \rho g_r$$

$$+ \mu \left\{ \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial (r V_r)}{\partial r} \right] + \frac{1}{r^2} \frac{\partial^2 V_r}{\partial \theta^2} - \frac{2}{r^2} \frac{\partial V_\theta}{\partial \theta} + \frac{\partial^2 V_r}{\partial z^2} \right\} \quad (r)$$

$$\rho \left(\frac{\partial V_\theta}{\partial t} + V_r \frac{\partial V_\theta}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_\theta}{\partial \theta} + \frac{V_r V_\theta}{r} + V_z \frac{\partial V_\theta}{\partial z} \right) = -\frac{1}{r} \frac{\partial p}{\partial \theta} + \rho g_\theta$$

$$+ \mu \left\{ \frac{\partial}{\partial r} \left[\frac{1}{r} \frac{\partial (r V_\theta)}{\partial r} \right] + \frac{1}{r^2} \frac{\partial^2 V_\theta}{\partial \theta^2} + \frac{2}{r^2} \frac{\partial V_r}{\partial \theta} + \frac{\partial^2 V_\theta}{\partial z^2} \right\} \quad (\theta)$$

$$\rho \left(\frac{\partial V_z}{\partial t} + V_r \frac{\partial V_z}{\partial r} + \frac{V_\theta}{r} \frac{\partial V_z}{\partial \theta} + V_z \frac{\partial V_z}{\partial z} \right) = -\frac{\partial p}{\partial z} + \rho g_z$$

$$+ \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial V_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 V_z}{\partial \theta^2} + \frac{\partial^2 V_z}{\partial z^2} \right] \quad (z)$$

The shear stresses for a Newtonian fluid in cylindrical polar coordinates are:

$$\tau_{r\theta} = \tau_{\theta r} = \mu \left[r \frac{\partial}{\partial r} \left(\frac{V_\theta}{r} \right) + \frac{1}{r} \frac{\partial V_r}{\partial \theta} \right] \quad \tau_{\theta z} = \tau_{z\theta} = \mu \left(\frac{\partial V_\theta}{\partial z} + \frac{1}{r} \frac{\partial V_z}{\partial \theta} \right) \quad \tau_{rz} = \tau_{zr} = \mu \left(\frac{\partial V_r}{\partial z} + \frac{\partial V_z}{\partial r} \right)$$